Amendments to the Specification:

Please replace paragraphs 2 and 3, on page 9, with the following replacement paragraphs:

In one embodiment, the present invention relates to a process for purification of at least one cyclosiloxane precursor comprising at least water and optionally at least one other impurity selected from acidic and basic impurities, said cyclosiloxane comprising the formula $[R R' Si\text{-}O]_n$, wherein each of R and R^1 is same or different and independently selected from the group consisting of hydrogen, C_1-C_8 alkyl, C_1-C_8 alkoxy, C_1-C_8 alkene, C_1-C_8 alkyne, and C_1-C_8 carboxyl; and n is from 2 to 8, said process comprising contacting the cyclosiloxane material with an adsorbent bed material, so as to remove at least a portion of the water and optionally a portion of the acidic **and/or basic** impurity therefrom.

As used herein an adsorbent ~~and~~ or drying agent is defined as a substance that absorbs water and/or other impurities. Drying agents ~~and/or~~ adsorbents are grouped into two major classes: chemically acting and physically acting drying agents.

Please replace the last paragraph, on page 11, with the following replacement paragraph:

In a further embodiment the adsorbent bed may be integrated in the form of a column. The column may for example have a volume in the range of from about 1 to 50 liters and preferably from 2 to 10 liters. The cyclosiloxane to be purified may be pumped or gravity fed through the column and into a flask. The adsorbent bed is most desirably incorporated in the form of a column through which the TMCTS can be pumped. An example of an adsorbent bed in a column, for instance is one in which the adsorbent bed has a cross-sectional area of from about 0.1 to 20 inches and preferably from 0.5 to 4, and about 1 of 10% molecular sieves. The above data on a typical adsorbent bed is not given for any purpose of limiting the instant invention, it is given for the purpose of illustrating a typical bed of adsorbent molecular sieves that can be utilized within the scope of the instant invention. The TMCTS then is pumped or gravity fed through the adsorbent bed to obtain a product having a reduced level of acidic **and/or basic** impurity or water. Generally, the adsorbent process is preferably carried out anywhere at a temperature of from about 0°C to 35°C. It is undesirable to carry out the adsorbent process at a temperature of the adsorbent bed above 35°C., since the

adsorption may not be as efficient at that point. Further, the acidic **and/or basic** impurities may tend to vaporize at temperatures above that level. With respect to the 0 °C. lower limit, the only reason the lower limit appears is that it is difficult to refrigerate an adsorbent bed below the 0°C. level. However, temperatures below 0 °C. for the adsorbent bed could be utilized to carry out the adsorption process therewith. Preferably, the adsorption process is carried out at room temperature since this does not require refrigeration. It should be pointed out that before the TMCTS is passed through the adsorbent bed, it is desirable that the TMCTS be purified as much as possible by distillation so that the impurities easily separated by distillation are not present in the TMCTS stream and thus become adsorbed on the adsorbent bed, saturating it with impurities, thus, shortening its useful life. Accordingly, it is highly desirable that the TMCTS before it is passed through the adsorbent bed, be purified by distillation once, twice or more times before it is subjected to the instant process. The residence time of the stream of TMCTS in the adsorbent bed will vary with practice. It has been found that a residence time of as little as 0.5 hours in the adsorbent bed will remove a substantial amount of water and/or **basic and/or** acidic impurities while a maximum time of 10 hours will more completely purify the stream of TMCTS.

Please replace paragraph 1, on page 15, with the following replacement paragraph:

In one embodiment, the concentration of water in the original cyclosiloxane to be purified **is measured** by analytical methods known to those skilled in the art, including but not limited to: Karl Fisher titration, gas chromatography, Fourier Transform Infrared spectroscopy, etc. Such analysis provides for a more precise measurement as to the volume of the azeotropic component or adsorbent material necessary to remove the required portion of the water and/or acidic impurity.